

Coupling amine storage tanks in coal fired power plants with renewable electricity generation

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Motivation

- An amine-based Carbon Capture and Storage system CCS, consists of two main elements: an absorber where CO₂ is removed, and a regenerator where CO₂ is released and the original solvent - monoethanol amine (MEA) - is recovered
- Approximately 55% of the CCS energy penalty is due to the steam consumption of the regenerator and 35% is due to the compression of the captured CO₂ for transport to the storage site
- In a "CCS with Amine Storage" system the quantity of CO₂ captured remains the same as in a conventional amine-based system, but unlike in conventional CCS setups, the stripping of the CO₂-rich amine solution and compression of the CO₂ only occur during "off-peak" hours, when the cost of energy use is comparatively low
- The CO₂-rich amine solution that is not stripped down during times of high energy cost is temporarily stored in a tank. An additional regenerated amine storage tank is required to supply regenerated amine to the absorber when the regenerator is turned off
- A renewable source can provide electricity and/or steam for solvent regeneration and compression so that the original power output of the coal plant does not change and can be sold at peak hours
- The amine storage tanks allow the use of renewable energy when it is available. In this way the integration cost of renewable energy can be reduced.

Objectives

1. Explore whether the benefits of amine-storage from price arbitrage in US electricity markets outweigh its capital costs
2. Find a threshold for the capital cost of a source of renewable power so that the economic benefits of the whole CCS storage system with renewable generation outweigh its cost

METHOD

P_k : Kth lowest electricity hourly price of the day (\$/kWh)

m-th Daily Price Differential : $DPD_m = \sum_{k=24-m+1}^{24} \frac{P_k}{m} - \sum_{k=1}^{24-m} \frac{P_k}{24-m}$

E : CCS Energy use that can be differed with storage system (kWh/hour).

H_s : Number of hours the system operates in storage mode (hours/day). Same as Capacity of the storage system.

CF : Capacity factor of coal plant.

$CC_{H_s}^S$: Annualized Capital Cost of Storage with H_s capacity (\$)

A storage system with capacity H_s is cost effective if:

$$DPD_{H_s} > \frac{CC_{H_s}^S}{E \times 365 \times H_s \times CF}$$

METHOD CONT'D

m-th Daily Low Price Sum : $DLS_m = \sum_{k=1}^{24-m} P_k$

$CC_{H_s}^R$: Annualized Capital Cost of Renewable Generator that supplies all the power for regeneration and compression in a system with H_s hours of rich amine storage

A storage system of capacity H_s with renewable energy for regeneration and compression is cost effective if:

$$CC_{H_s}^R \leq 365 \times E \times (DPD_{H_s} \times H_s \times CF + DLS_{H_s}) - CC_{H_s}^S$$

RESULTS

Capital Cost of Storage MEA Inventory and storage tank

- MEA cost: 630 – 711 \$/m³
 - Circulation rate: 15-19 m³/hour/MW
 - MEA inventory: circulation rate * H_s
- For 500MW plant with $H_s = 1$, upper estimate:
MEA: \$6.7M, stainless steel tank: \$3.3M

Oversized CCS components

- Most of the components (excluding the absorber) need to be scaled up in capacity by $24/(24-H_s)$
- For a retrofit plant with 303MW-net (NETL study),
 $H_s=1$, cost = \$15.8M . $H_s=4$, cost = \$67.1M
For a new supercritical plant with 512MW-net, $H_s=1$,
cost = \$89.1M. $H_s=4$, cost \$163.9M

Required Daily Price Differential for a storage-only retrofit plant

Capacity Factor	Required DPD (\$/MWh)	
	Hs=1	Hs=4
1	41.20	43.73
0.95	43.36	46.04
0.9	45.77	48.59
0.85	48.47	51.45
0.8	51.49	54.67

Assuming:

- E=118MWh;
- Capital Charge Factor = 11.28%

Observed average DPD

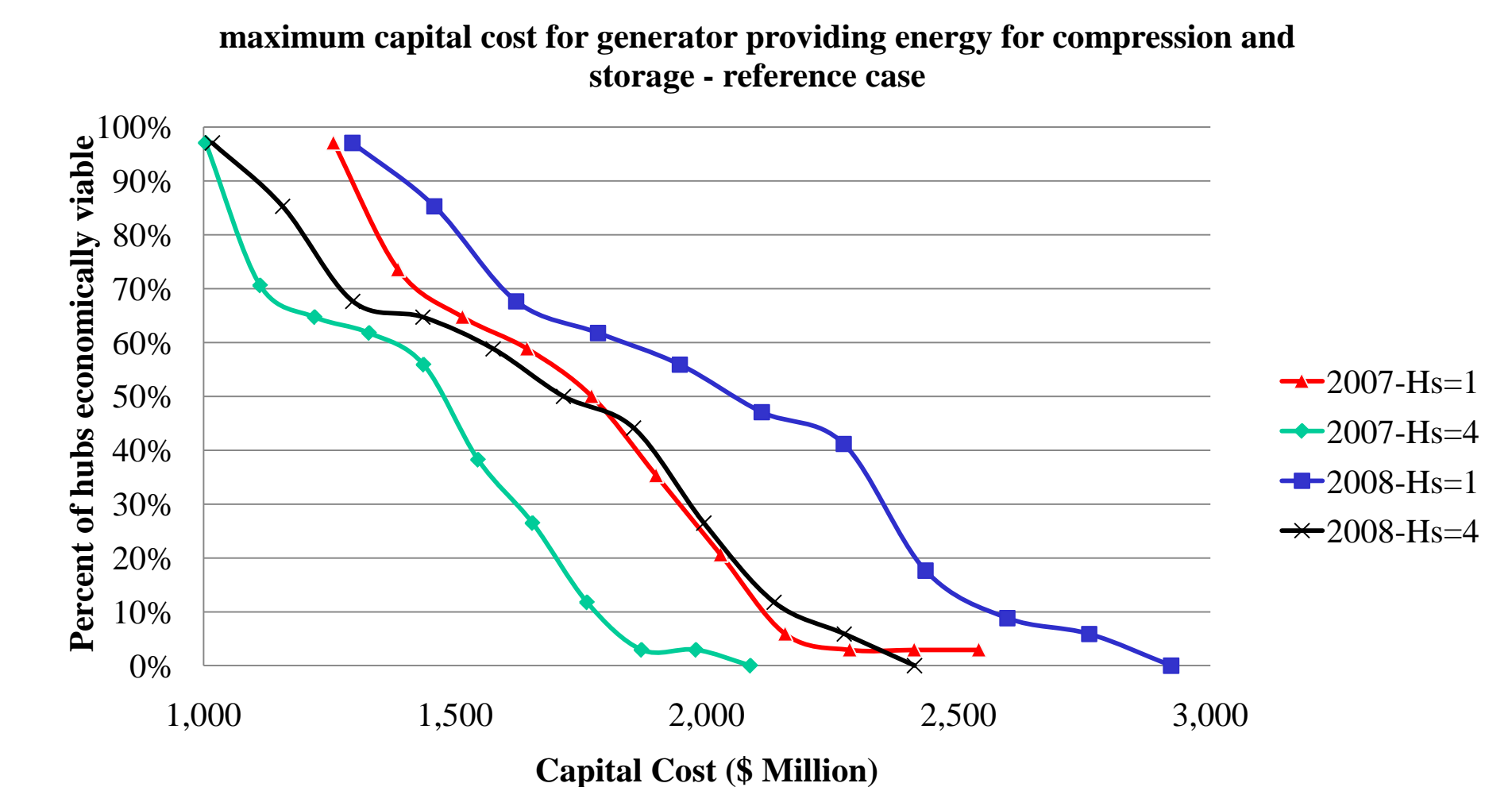
	2007		2008	
	Hs=1	Hs=4	Hs=1	Hs=4
NIEMO				
CAPITL Zone	\$ 24.63	\$ 22.11	\$ 27.92	\$ 24.82
CENTRL Zone	\$ 21.94	\$ 20.08	\$ 25.20	\$ 22.45
DUNWOD Zone	\$ 33.54	\$ 30.37	\$ 40.43	\$ 36.98
GENESE Zone	\$ 21.42	\$ 19.64	\$ 24.45	\$ 21.78
WEST Zone	\$ 20.20	\$ 18.47	\$ 21.26	\$ 18.99
HUD VL Zone	\$ 28.58	\$ 27.22	\$ 36.86	\$ 33.58
LONGIL Zone	\$ 43.38	\$ 38.08	\$ 44.91	\$ 40.94
MHK VL Zone	\$ 22.73	\$ 20.85	\$ 26.02	\$ 23.23
MILLWD Zone	\$ 33.45	\$ 30.29	\$ 40.06	\$ 36.65
N.Y.C. Zone	\$ 33.79	\$ 30.64	\$ 39.81	\$ 37.53
NORTH Zone	\$ 21.18	\$ 19.35	\$ 23.45	\$ 20.76
Cinergy Hub	\$ 37.28	\$ 33.45	\$ 39.05	\$ 35.47
FE Hub	\$ 37.55	\$ 33.56	\$ 38.76	\$ 35.24
Illinois Hub	\$ 37.55	\$ 33.77	\$ 37.77	\$ 34.63
Michigan Hub	\$ 38.88	\$ 34.50	\$ 40.54	\$ 36.77
Minnesota Hub	\$ 47.48	\$ 41.85	\$ 42.44	\$ 38.78
INDWEST				
Connecticut Zone	\$ 26.35	\$ 24.55	\$ 30.77	\$ 28.08
Maine Zone	\$ 19.99	\$ 17.48	\$ 22.63	\$ 20.10
NE MassBost Zone	\$ 21.85	\$ 19.14	\$ 24.65	\$ 22.30
New Hampshire Zone	\$ 21.10	\$ 18.80	\$ 24.23	\$ 21.82
Rhode Island Zone	\$ 20.90	\$ 18.51	\$ 24.37	\$ 21.92
SE MASS Zone	\$ 19.85	\$ 18.82	\$ 25.43	\$ 22.96
WC MASS Zone	\$ 22.09	\$ 19.78	\$ 25.43	\$ 22.96
Vermont Zone	\$ 22.46	\$ 20.22	\$ 24.98	\$ 22.63
REP GEN HUB	\$ 29.75	\$ 28.20	\$ 31.04	\$ 29.87
REP-DAYTON HUB	\$ 31.19	\$ 29.72	\$ 32.78	\$ 31.71
CHICAGO GEN HUB	\$ 31.13	\$ 29.64	\$ 33.43	\$ 32.51
CINCINNATI HUB	\$ 31.13	\$ 29.64	\$ 34.14	\$ 33.22
DOMINION HUB	\$ 32.94	\$ 31.24	\$ 36.52	\$ 34.82
EASTERN HUB	\$ 36.37	\$ 34.10	\$ 45.21	\$ 41.41
ILLINOIS HUB	\$ 31.38	\$ 29.89	\$ 33.75	\$ 32.84
NEW JERSEY HUB	\$ 35.99	\$ 33.72	\$ 42.91	\$ 39.61
OHIO HUB	\$ 31.09	\$ 29.58	\$ 32.89	\$ 31.81
WEST INT HUB	\$ 29.13	\$ 27.63	\$ 31.55	\$ 30.58
WESTERN HUB	\$ 32.37	\$ 31.04	\$ 40.13	\$ 37.82

hubs where storage-only is economic are highlighted

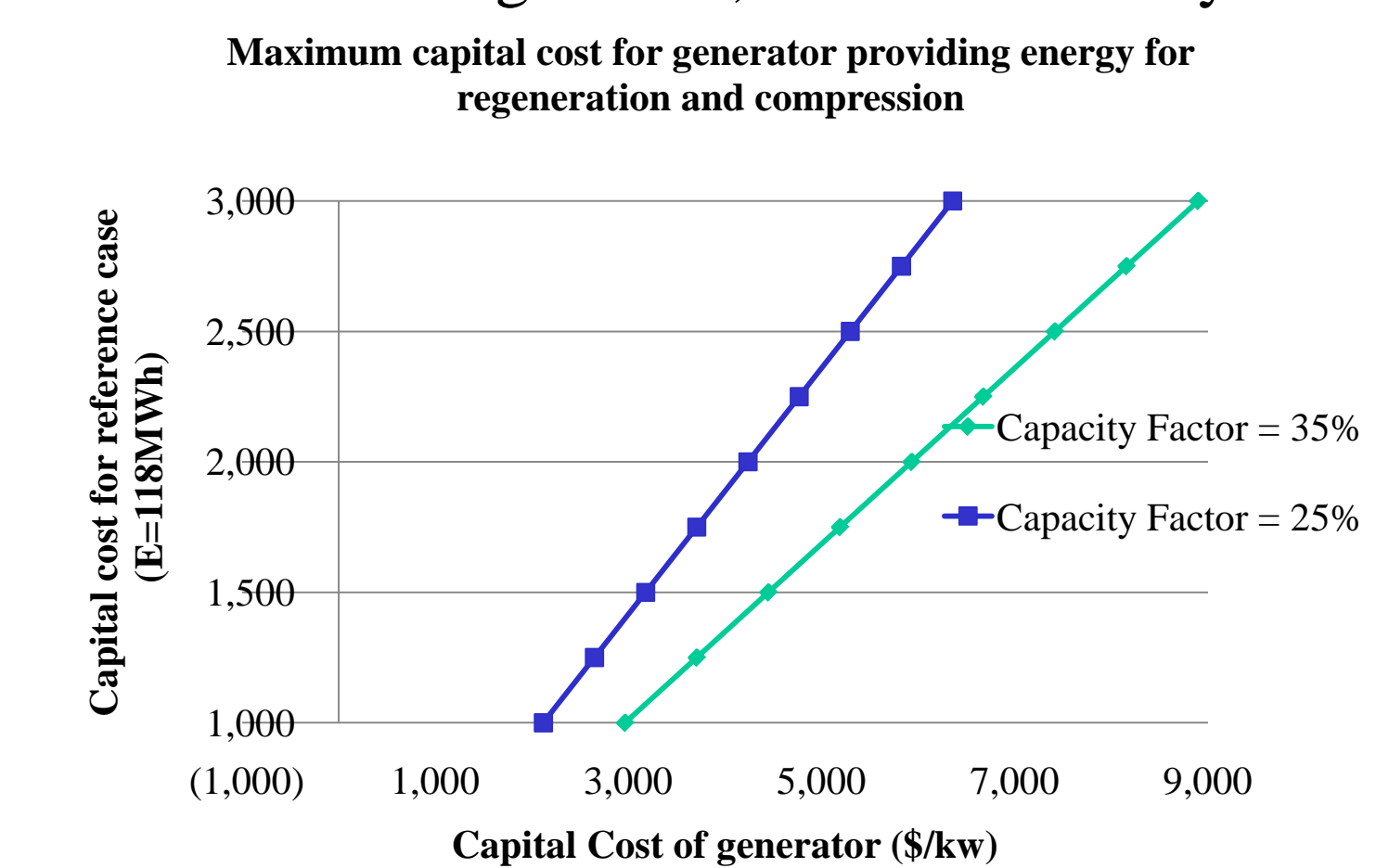
RESULTS CONT'D

Finding a threshold for the Capital Cost of a generator supplying energy for regeneration and compression

The figure below shows the maximum capital cost of a generator supplying an average of 118MWh per hour, for a CCS plant with 1 and 4 hours of amine storage, according to electricity prices observed in 35 hubs during 2007 and 2008.



Assuming the least favorable electricity prices observed, and a capacity factor of 25% the threshold for the capital cost of a generator providing energy for amine regeneration and compression is 2,912 \$/kw for a system with 1 hour of storage and 2,127 \$/kw for a system with 4 hours of storage:



CONCLUSIONS AND WORK IN PROGRESS

- The economic benefits of price arbitrage allowed by amine storage do not outweigh its costs, but integration with a renewable source is economically viable
- Research is underway to explore the optimal configuration of a system that combines amine storage with electrical power and/or steam from wind and thermal solar. Monte Carlo simulation of wind speeds and electricity prices for a case study show system is likely to be profitable

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